

reacting said hydrocarbon mixture containing olefins and having a boiling range within the range of  $C_4$  to  $250^{\circ} C$ , and a sulfur content of at least 150 ppm with hydrogen in the presence of a catalytic composition comprising:

a) an acidic carrier consisting of a silica and alumina gel, amorphous to X-rays, with a molar ratio  $SiO_2/Al_2O_3$  of 30/1 to 500/1, having a surface area ranging from 500 to 1000  $m^2/g$ , a porosity of 0.3 to 0.6 ml/g and a pore diameter within the range of 10-40 Å;

b) a mixture of metals belonging to Groups VIB and VIII of the Periodic Table deposited on the carrier in an overall quantity ranging from 2 to 67 % by weight with respect to the total amount of components (a) + (b), thereby effecting said hydrodesulfurization with concomitant skeletal isomerization of the olefins of said mixture. ✓

17. (Amended) The process according to Claim 1, wherein the hydrocarbon mixture which is subjected to hydrodesulfuration is a mixture that boils within the range of  $C_5$  to  $220^{\circ} C$ .

18. (Amended) The process according to Claim 1, wherein the catalyst is activated by sulfidation.--

Please add new Claim 27 as follows:

--27. (Newly Added) The process according to Claim 1, wherein the hydrocarbon mixture is a full range naphtha having a boiling range of  $35^{\circ}$  - $250^{\circ} C$ . --

#### **REMARKS**

Claims 1-18 and newly added Claim 27 are active in the case. Reconsideration is respectfully requested.